

NEXT GENERATION NITRIC ACID PRODUCTION



Paz Muñoz

AGENDA

01 INTRODUCTION

02 TOTAL RECYCLE CONCEPT

03 OXYGEN SUPPLY

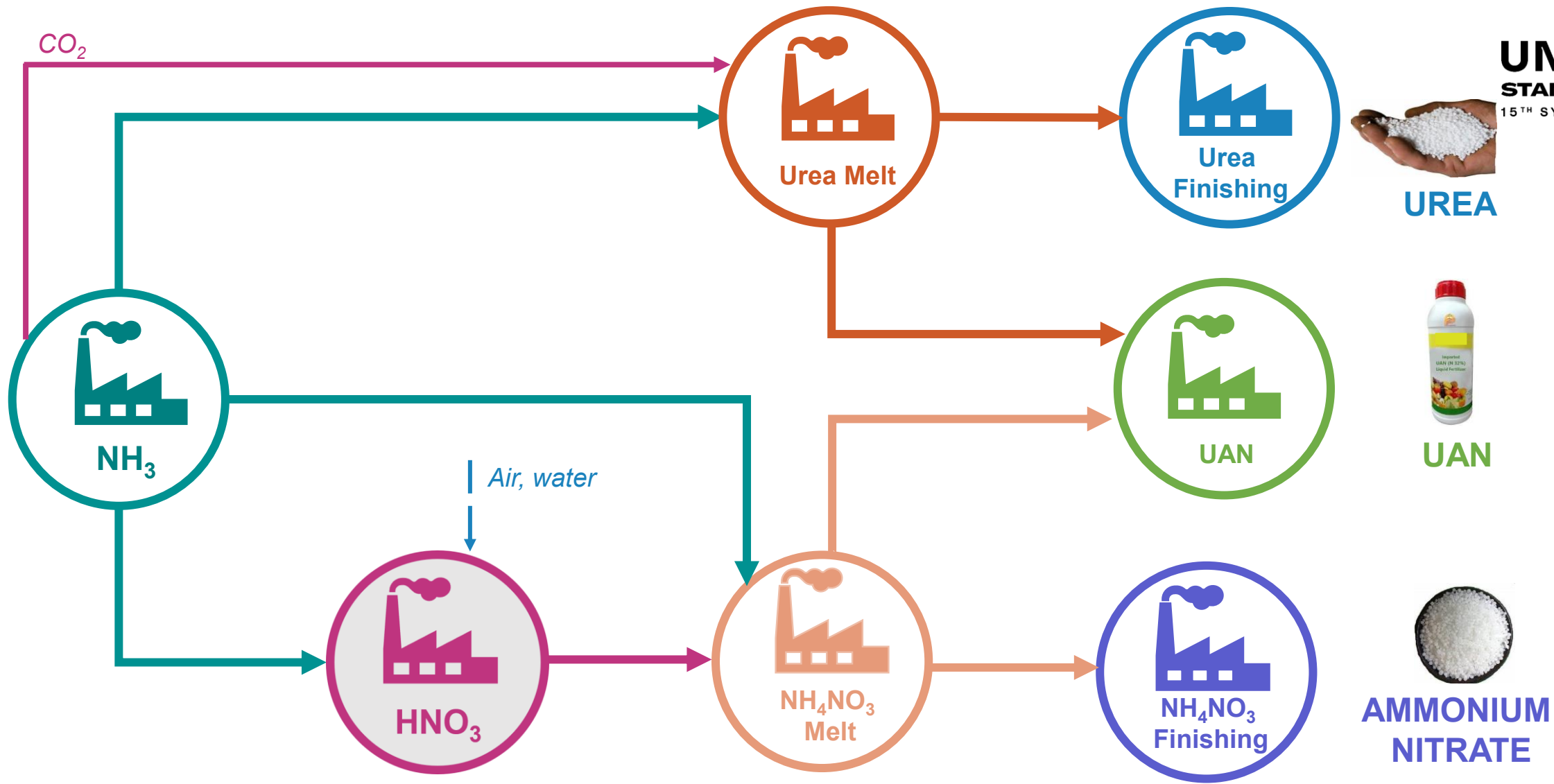
04 ECONOMICS

05 CONCLUSIONS



INTRODUCTION

AMMONIA TO FERTILIZERS

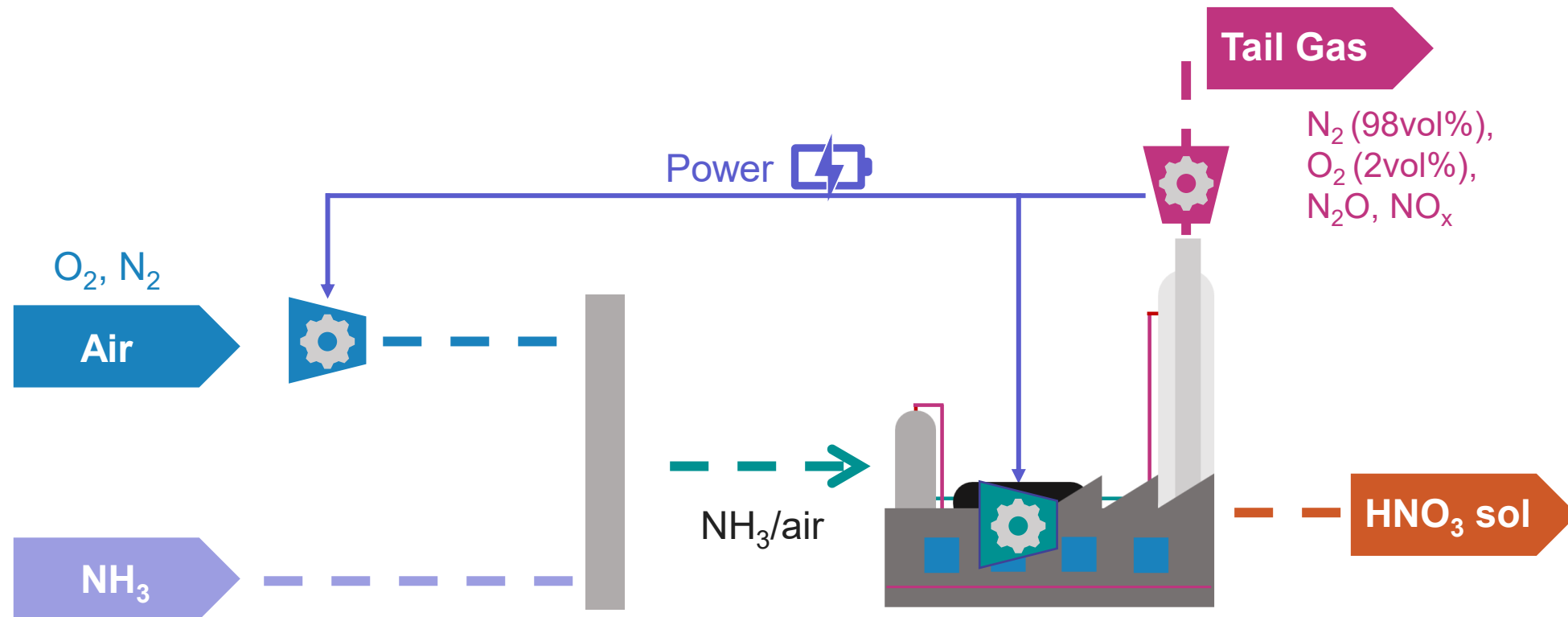


UNFOLD
STAMICARBON
15TH SYMPOSIUM 2026

HOW IS NITRIC ACID PRODUCED?



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STAMI NITRIC ACID PRODUCTION TECHNOLOGIES



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	MONO PRESSURE	DUAL PRESSURE
Capacity		
N. Equipment		
CAPEX		
OPEX		

STAMI NITRIC ACID PRODUCTION TECHNOLOGIES



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High Energy Efficiency

> 800kg
steam/ton HNO₃

Low NO_x/N₂O Emissions

<20ppm(vol)

Long lifetime

Low Corrosion Rates

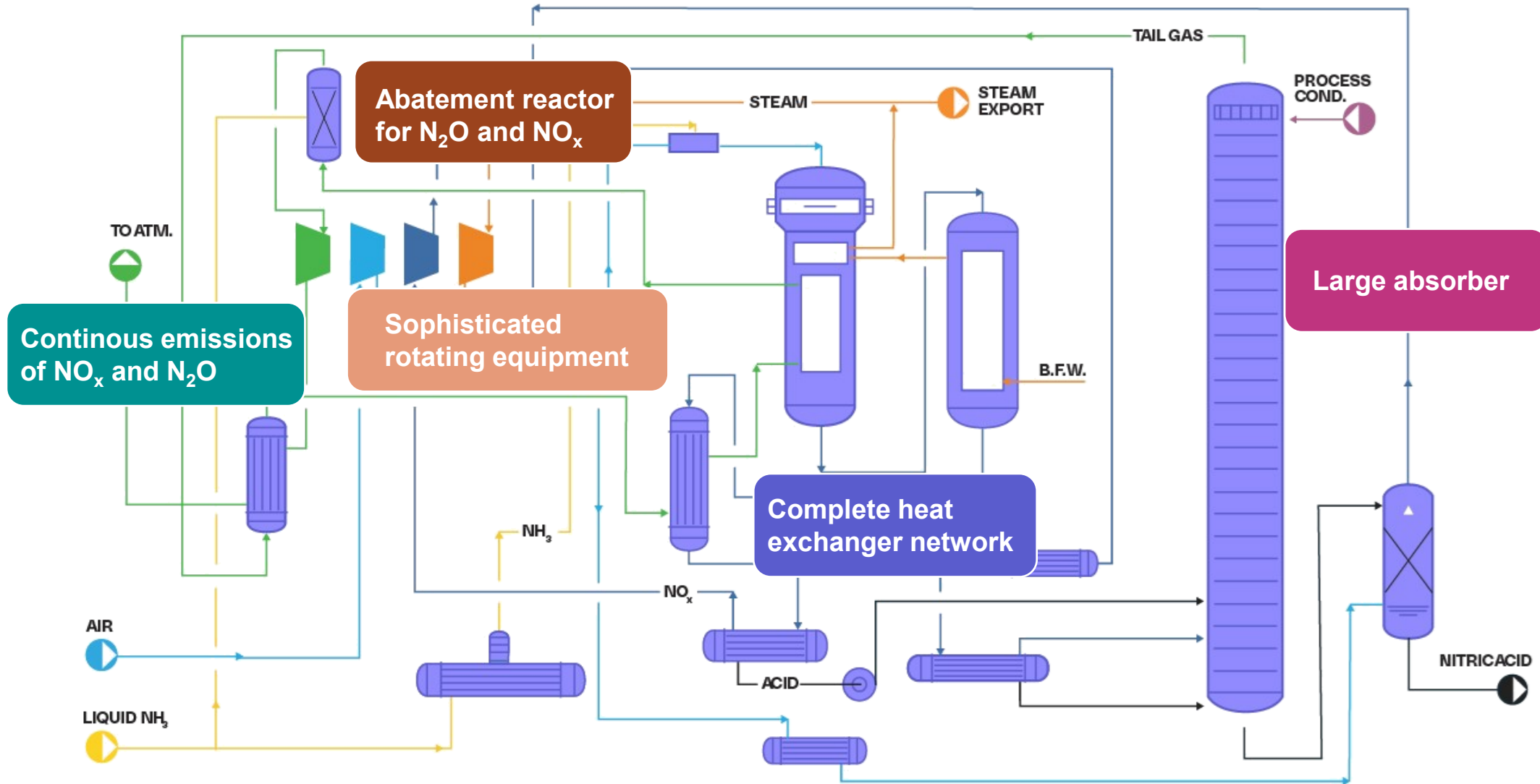
More power Tertiary abatement technology extracted in the tail gas expander
Pinch-optimized HX layout. **Smaller** catalyst bed **Minimizing** condensation/(re)evaporation effect
No addition of natural gas due to high tail gas temperature (480°C): **No use of exotic materials**



STANDARD NITRIC ACID PRODUCTION



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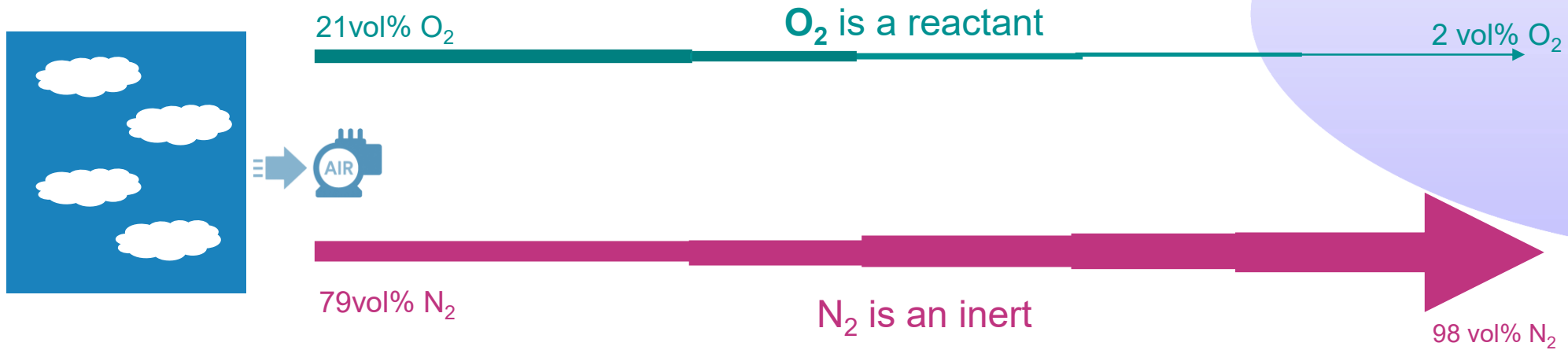
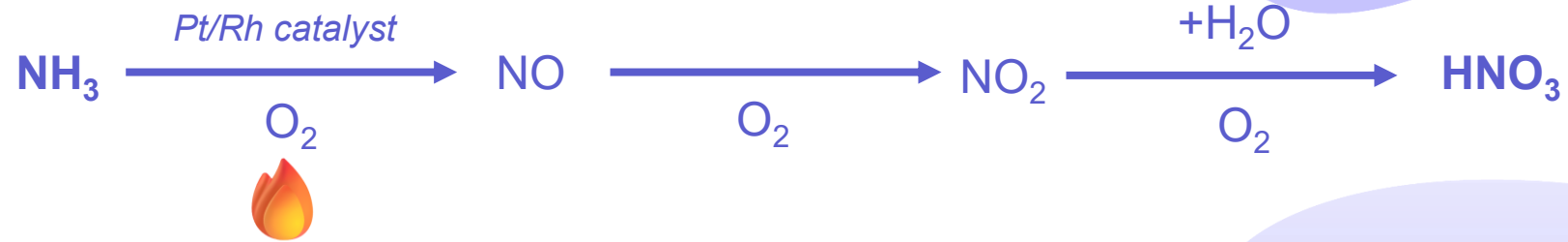


TOTAL RECYCLE CONCEPT

HOW IS NITRIC ACID PRODUCED?



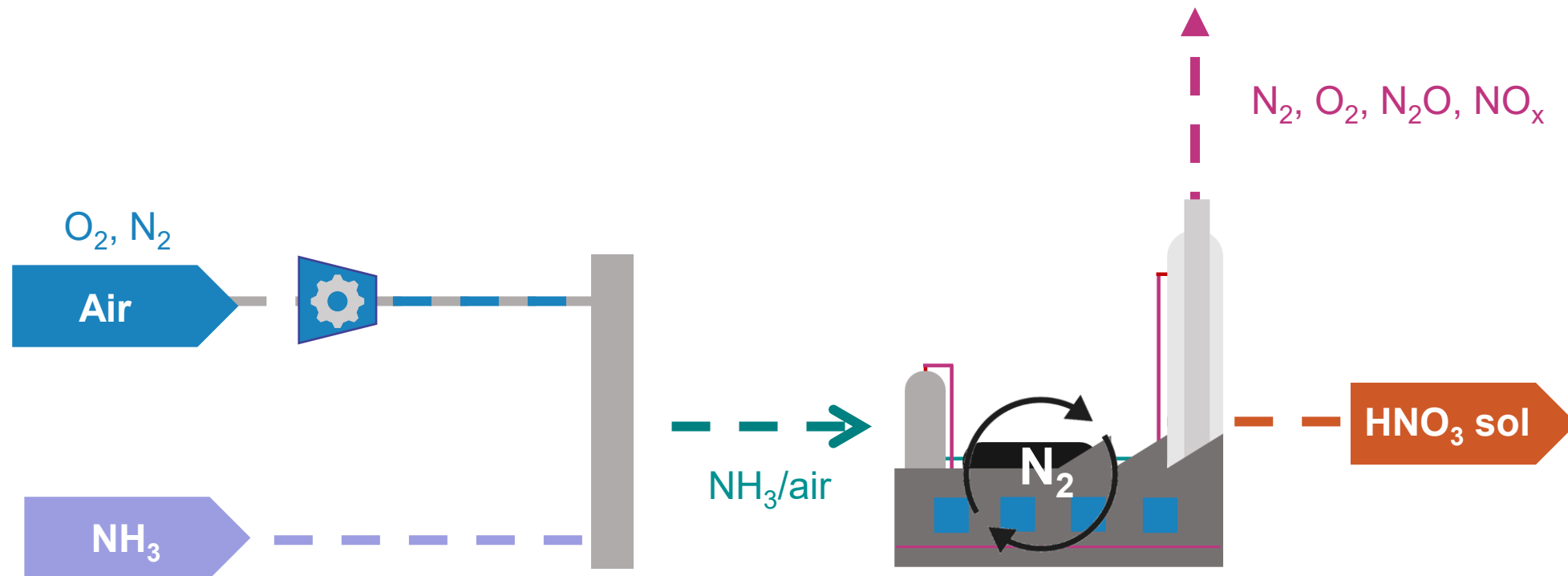
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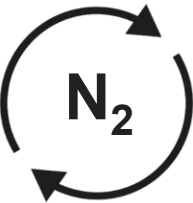
TOTAL RECYCLE CONCEPT



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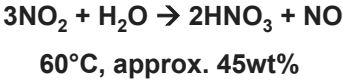
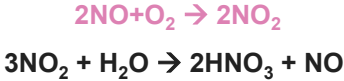
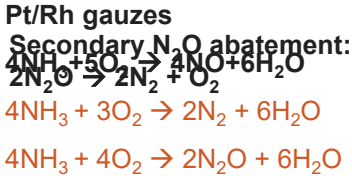
TOTAL RECYCLE CONCEPT



900°C



O_2/N_2 mixture

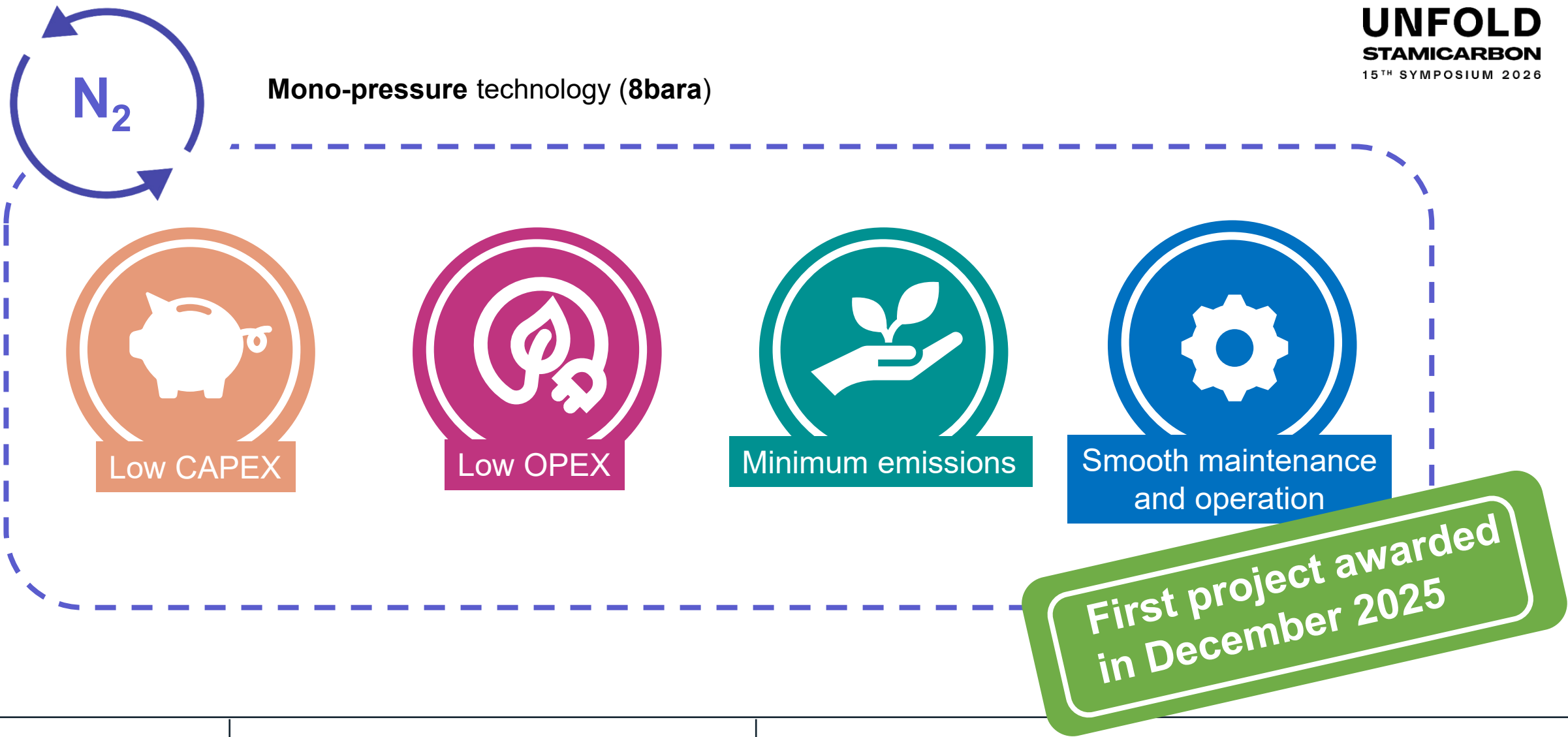


Process gas with
high O_2 content

TOTAL RECYCLE CONCEPT



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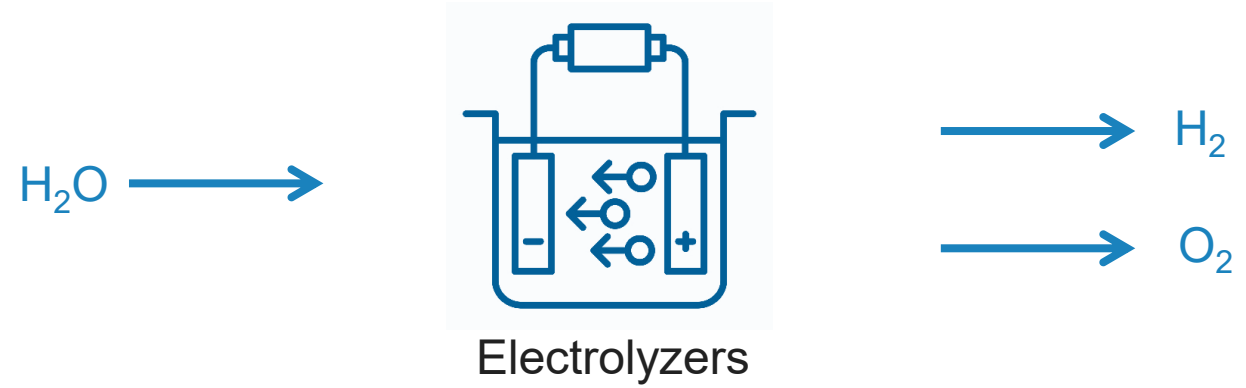
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OXYGEN SUPPLY

OXYGEN SUPPLY



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THE COLORS OF AMMONIA PRODUCTION



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Natural gas/**Coal** as feedstock
(SMR/coal gasification/POX)



Natural gas as feedstock with **CO₂ capture**
(usually CPO or ATR technologies that include ASU)



Electrolysis powered by **nuclear energy**

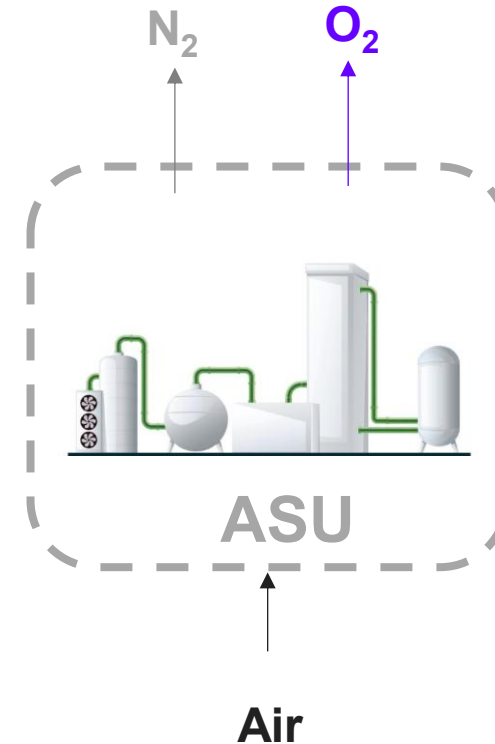


Electrolysis powered by **renewable energy**

THE COLORS OF AMMONIA PRODUCTION



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Air Separation Unit is already required for coal gasification and ATR/CPO technologies.

Unit can be **scaled up** to supply O₂ to Nitric acid plant.

THE COLORS OF AMMONIA PRODUCTION



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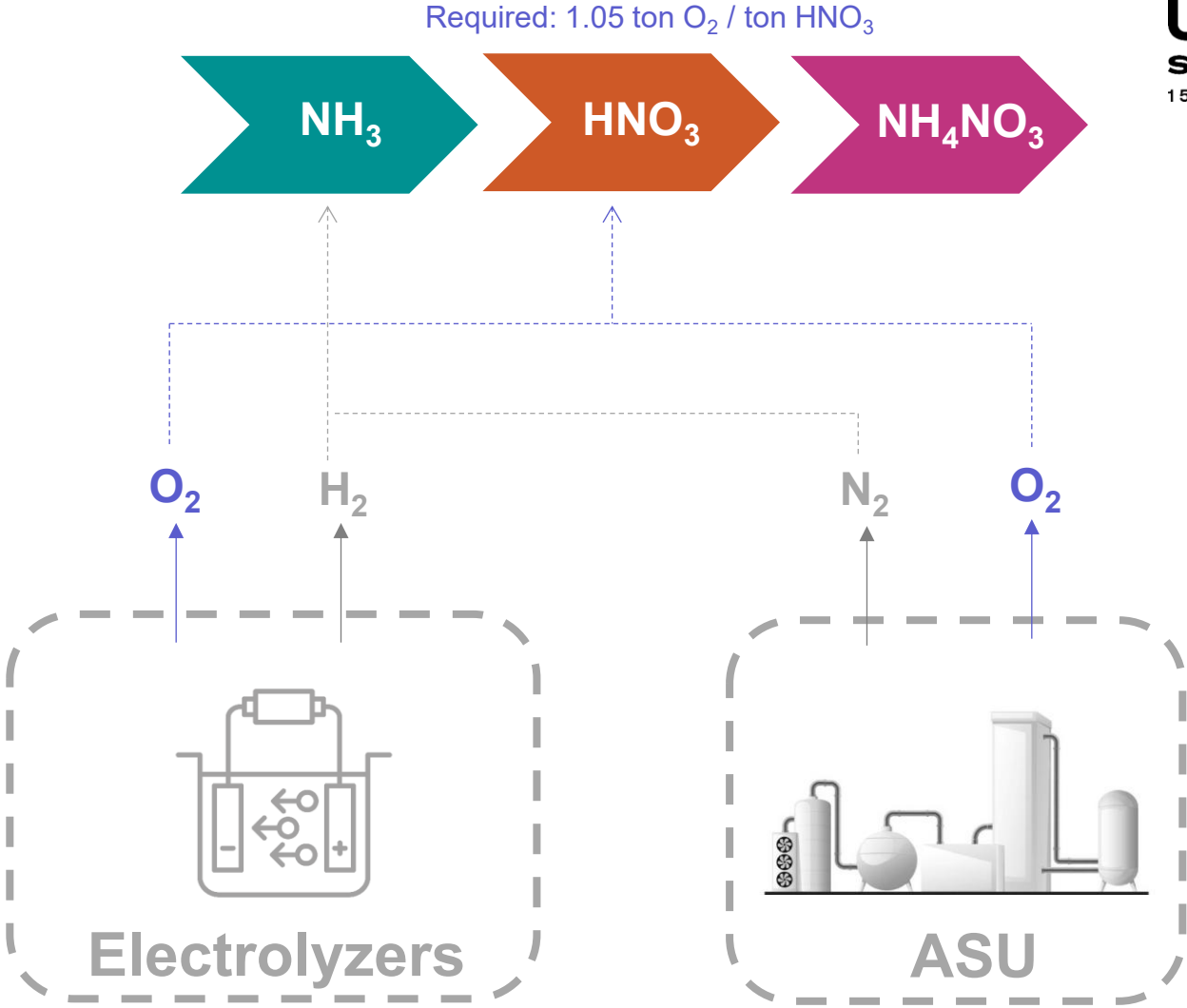
Grey

Brown

Blue

Pink

Green





ECONOMICS



Case Study 1: 325 MTPD



mono-pressure

VS



total recycle

**Total Recycle
reduces CAPEX
up to 30%**

**Total Recycle reduces
CAPEX up to 40%**



dual-pressure

VS



total recycle

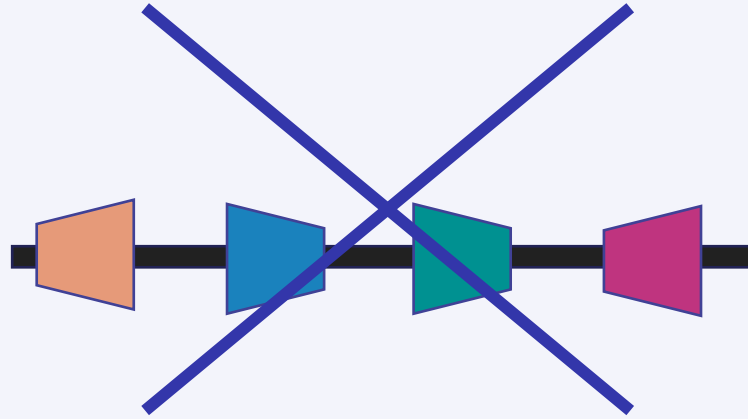
Case Study 2: 1000 MTPD

*Based in EU

MAIN ADVANTAGES INFLUENCING CAPEX



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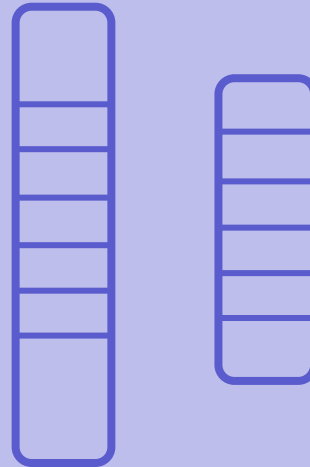
No compressor train



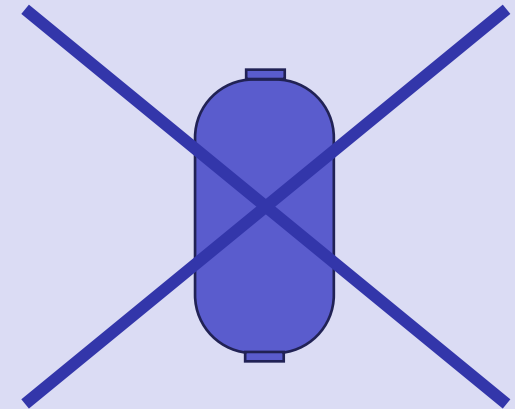
Wide range of capacities



Simplified heat
exchanger network



Oxidation/absorption column
40% reduced in length



No need for NO_x
abatement reactor

OPEX ANALYSIS



mono-pressure

VS



total recycle

Total Recycle reduces OPEX up to 25%

Total Recycle reduces OPEX up to 20%



dual-pressure

VS

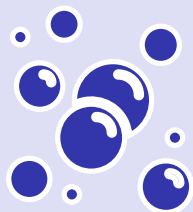


total recycle

*Based in EU

Assumption: O₂ is considered to be received pressurized and at no cost

MAIN ADVANTAGES INFLUENCING OPEX



High Steam Export (45bar, 450°C)

1200kg steam/ton HNO_3 (100%)

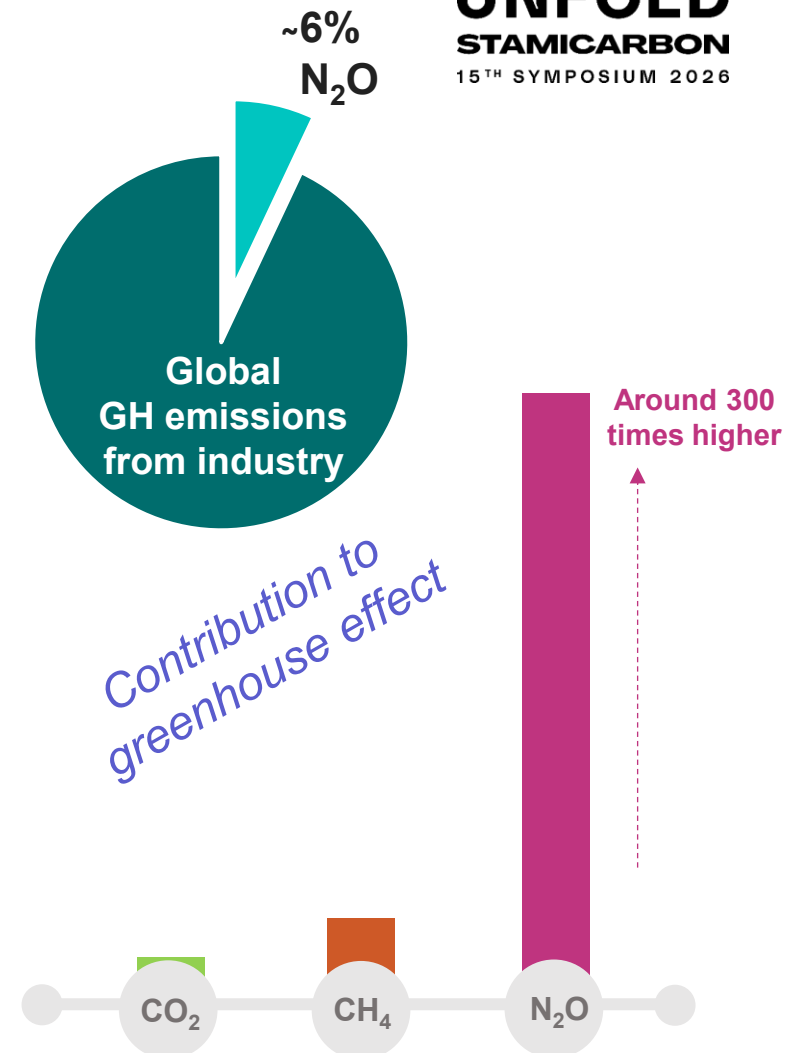
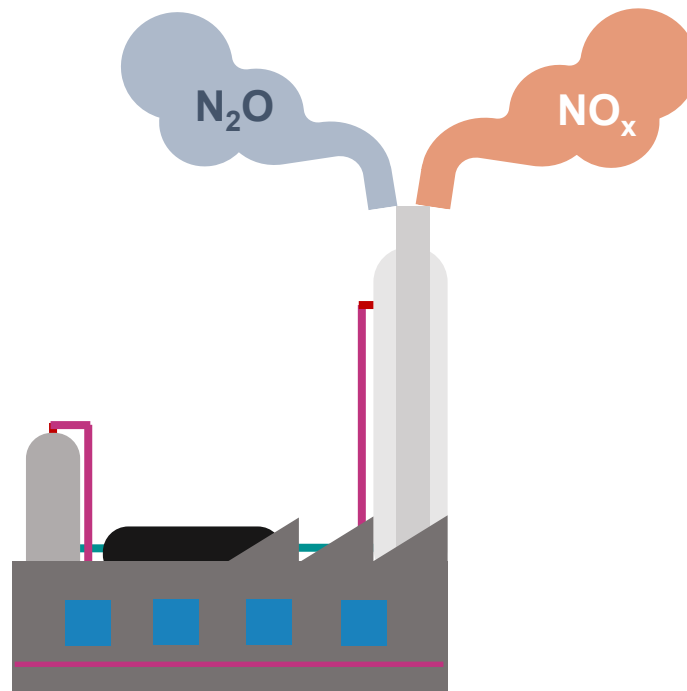
~50% above best conventional plants



Minimum Emissions

< 4 g N_2O /ton HNO_3 (100%)

< 4 g NO_x /ton HNO_3 (100%)



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MAIN ADVANTAGES INFLUENCING OPEX



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High Steam Export (45bar, 450°C)

1200kg steam/ton HNO₃ (100%)

~50% above best

STANDARD TECHNOLOGY

Considering tertiary abatement
system

- 10 ppmv NO_x → 50 g/ton HNO₃
- 20 ppmv N₂O → 120 g/ton HNO₃

N₂O → CO₂ credits



Minimum Emissions

< 4 g N₂O/ton HNO₃ (100%)
< 4 g NO_x/ton HNO₃ (100%)

MAIN ADVANTAGES INFLUENCING OPEX



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High Steam Export (45bar, 450°C)

1200kg steam/ton HNO₃ (100%)

~50% above best conventional plants

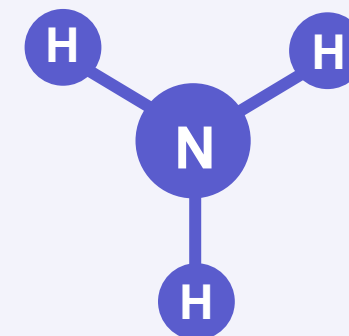


Minimum Emissions

< 4 g N₂O/ton HNO₃ (100%)

< 4 g NO_x/ton HNO₃ (100%)

Smooth **operation** and
maintenance
(low corrosion rates)



Lower **ammonia**
consumption

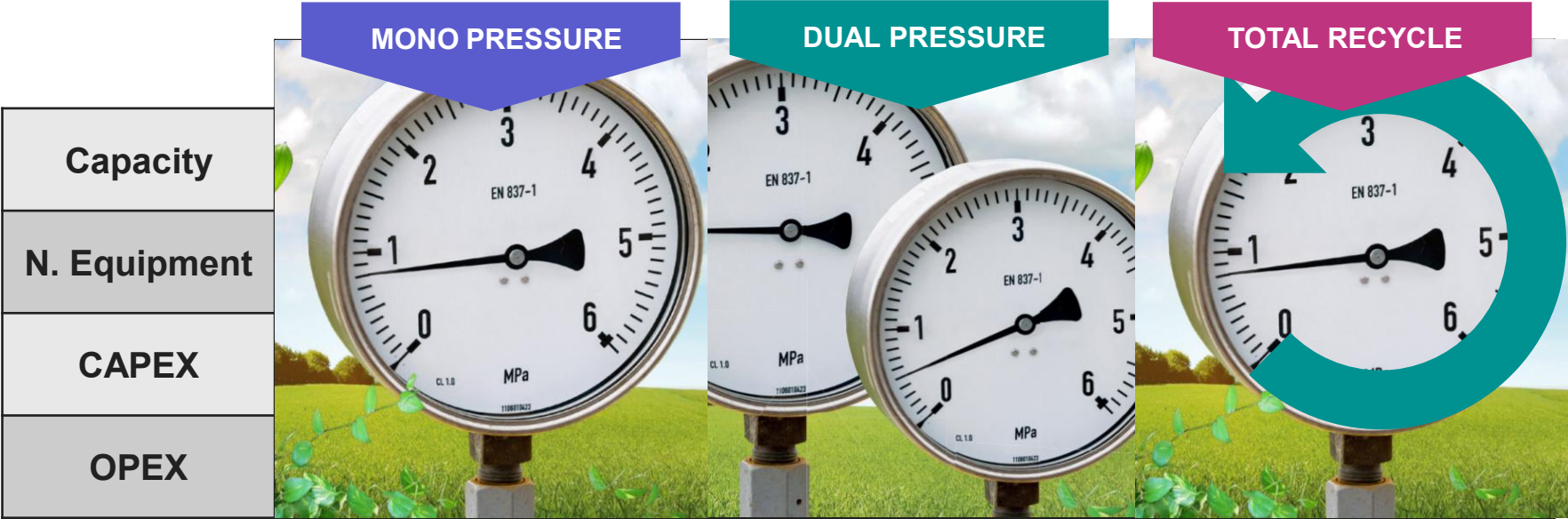
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CONCLUSION

CONCLUSION



CONCLUSION



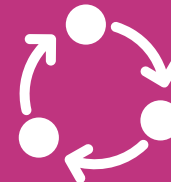
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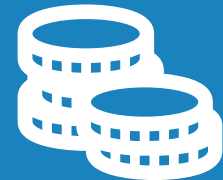
Stamicarbon is contributing to the **decarbonization** of the fertilizer industry



Process synergies enable development of **new eco-friendly** processes



First award for **Total Recycle concept** in December 2025



Total Recycle Concept delivers up to **40% reduction in CAPEX** and **25% savings in OPEX**

THANK YOU

